

AMENDMENTS TO THE CLAIMS:

The following listing of claims replaces all prior listings, and all prior versions, of claims in the application:

Listing of Claims:

1. (currently amended) An apparatus for continuously producing polycarbonate, comprising:

a first reactor which is a uniaxial horizontal agitation reactor without any agitator center shaft, having a liquid viscosity range from ~~4 Pa·S~~ 1 Pa·s to ~~1,000 Pa·S~~ 1,000 Pa·s and adapted to be supplied with a mixed liquid of diphenyl carbonate and alcohol, for agitating said mixed liquid to increase the liquid viscosity of said mixed liquid; and

a second reactor which is a horizontal biaxial agitation reactor, having a liquid viscosity range from ~~400 Pa·S~~ 100 Pa·s to ~~5,000 Pa·S~~ 5,000 Pa·s and adapted to be supplied with said mixed liquid whose liquid viscosity has been increased in said first reactor, for agitating the supplied, mixed liquid to increase the liquid viscosity of the supplied, mixed liquid to continuously produce polycarbonate.

2. (currently amended) A method for continuously producing polycarbonate, comprising:

supplying a mixed liquid of diphenyl carbonate and alcohol to a first reactor which is a uniaxial horizontal agitation reactor without any agitator center shaft, having a liquid viscosity range from 1 Pa·s ~~1 Pa·S~~ to ~~1,000 Pa·S~~ 1,000 Pa·s;

agitating said mixed liquid in said first reactor to increase the liquid viscosity of

said mixed liquid;

supplying the agitated, mixed liquid from said first reactor to a second reactor which is a horizontal biaxial agitation reactor, having a liquid viscosity range from ~~100 Pa·s~~ 100 Pa·s to ~~5,000 Pa·s~~ 5,000 Pa·s; and

further agitating the supplied, mixed liquid in said second reactor to increase the liquid viscosity of the supplied, mixed liquid to continuously produce polycarbonate.

3. (currently amended) An apparatus for continuously producing polycarbonate, comprising:

a first reactor which is a uniaxial horizontal agitation reactor without any agitator center shaft, having a first liquid viscosity range from 1 Pa·s to 1,000 Pa·s and adapted to be supplied with a mixed liquid of diphenyl carbonate and alcohol, whose liquid viscosity is at an amount in a lower side of said first liquid viscosity range, for agitating said mixed liquid to increase the liquid viscosity of said mixed liquid; and

a second reactor which is a horizontal biaxial agitation reactor, having a second liquid viscosity range from an intermediate amount of said first liquid viscosity range to another amount higher than the highest amount of said first liquid viscosity range and adapted to be supplied with said mixed liquid whose liquid viscosity has been increased in said first reactor, for agitating the supplied, mixed liquid to increase the liquid viscosity of the supplied, mixed liquid to continuously produce polycarbonate.

4. (currently amended) A method for continuously producing polycarbonate, comprising:

supplying a mixed liquid of diphenyl carbonate and alcohol to a first reactor which is a uniaxial horizontal agitation reactor without any agitator center shaft, having a first liquid viscosity range from 1 Pa·s to 1,000 Pa·s;

agitating said mixed liquid in said first reactor to increase the liquid viscosity of said mixed liquid;

supplying the agitated, mixed liquid from said first reactor to a second reactor which is a horizontal biaxial agitation reactor, having a second liquid viscosity range from an intermediate amount of said first liquid viscosity range to another amount higher than the highest amount of said first liquid viscosity range; and

further agitating the supplied, mixed liquid ~~in~~ in said second reactor to increase the liquid viscosity of the supplied, mixed liquid to continuously produce polycarbonate.

5. (new) The apparatus according to claim 1, wherein said uniaxial horizontal agitation reactor includes a horizontal cylindrical vessel and agitation blades annularly distributed and successively arranged through the vessel and secured at positions deviated from a rotating axis toward an inner wall of the vessel without any agitator center shaft.

6. (new) The apparatus according to claim 5, wherein said horizontal biaxial agitation reactor has lattice blades.

7. (new) The method according to claim 2, wherein said uniaxial horizontal agitation reactor includes a horizontal cylindrical vessel and agitation blades annularly distributed and successively arranged through the vessel and secured at positions deviated from a rotating axis toward an inner wall of the vessel without any agitator center shaft.

8. (new) The method according to claim 7, wherein said horizontal biaxial agitation reactor has lattice blades.

9. (new) The apparatus according to claim 3, wherein said uniaxial horizontal agitation reactor includes a horizontal cylindrical vessel and agitation blades annularly distributed and successively arranged through the vessel and secured at positions deviated from a rotating axis toward an inner wall of the vessel without any agitator center shaft.

10. (new) The apparatus according to claim 9, wherein said horizontal biaxial agitation reactor has lattice blades.

11. (new) The method according to claim 4, wherein said uniaxial horizontal agitation reactor includes a horizontal cylindrical vessel and agitation blades annularly distributed and successively arranged through the vessel and secured at positions deviated from a rotating axis toward an inner wall of the vessel without any agitator center shaft.

12. (new) The method according to claim 11, wherein said horizontal biaxial agitation reactor has lattice blades.